

# inRAx



## MVI71-AFC

### PLC Platform

Gas and Liquid Flow Computer

## Calculation Test Report (EUB Test Cases)

December 13, 2005



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# Contents

|          |                           |           |
|----------|---------------------------|-----------|
| <b>1</b> | <b>INTRODUCTION .....</b> | <b>5</b>  |
| 1.1      | Test Assumptions .....    | 5         |
| 1.2      | Test Procedure .....      | 5         |
| <b>2</b> | <b>TEST CASES .....</b>   | <b>7</b>  |
| 2.1      | Test Case Number 1 .....  | 7         |
| 2.2      | Test Case Number 2 .....  | 9         |
| 2.3      | Test Case Number 3 .....  | 11        |
| 2.4      | Test Case Number 4 .....  | 13        |
| 2.5      | Test Case Number 5 .....  | 15        |
| 2.6      | Test Case Number 6 .....  | 17        |
| <b>3</b> | <b>CONCLUSION.....</b>    | <b>21</b> |



# 1 Introduction

## *In This Chapter*

- Test Assumptions..... 5
- Test Procedure..... 5

This document provides the MVI71-AFC test procedures and results in order to verify the MVI71-AFC AGA calculation results. The Alberta Energy and Utilities Board (EUB) uses the test cases presented in this document. The test cases are listed in the EUB Production Audit Handbook Guide 46, section 3.2 (January 2003).

## 1.1 Test Assumptions

The Alberta Energy and Utilities Board (EUB) used the AGA3 (1990) test procedure for Orifice Calculation (using metric units) and the compressibility factors calculated using AGA8 (1992). Although the MVI71-AFC uses the AGA3 report (1992) the results are not affected, since the values are calculated in the same way in both reports.

The orifice plate was assumed to be made of 316 SS

The ideal gas relative density was converted to the real gas relative density.

The calculated values were rounded to four decimal places, since the theoretical values are given using the same format (EUB Guide 46).

The MVI71-AFC variables that are not mentioned in this document were not changed during the tests. These variables had the default value when a new AFC project is created with the AFC Manager.

## 1.2 Test Procedure

The tests consisted on reading the output values generated by the MVI71-AFC module through the AFC manager software and comparing the calculated results with the EUB expected results. Each meter was configured using the AFC Manager software and the input variables (Temperature, Pressure and Differential Pressure) were entered through the ladder logic. Each meter was used to test a different test case:

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| <b>Meter Number</b> | <b>Test Case</b> |
|---------------------|------------------|
| 1                   | 1                |
| 2                   | 2                |
| 3                   | 3                |
| 4                   | 4                |
| 5                   | 5                |
| 6                   | 6                |

Follows below the configuration used during the tests:

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|                              |          |
|------------------------------|----------|
| Firmware version             | 2.02.000 |
| AFC Manager Software version | 2.02.000 |
| PLC processor                | PLC5/11  |

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## 2 Test Cases

### *In This Chapter*

|                            |    |
|----------------------------|----|
| ➤ Test Case Number 1 ..... | 7  |
| ➤ Test Case Number 2 ..... | 9  |
| ➤ Test Case Number 3 ..... | 11 |
| ➤ Test Case Number 4 ..... | 13 |
| ➤ Test Case Number 5 ..... | 15 |
| ➤ Test Case Number 6 ..... | 17 |

In order to verify the MVI71-AFC calculation program the EUB uses 6 test cases that are described in this section. This section shows all input parameters and calculated results for each test case.

### 2.1 Test Case Number 1

#### **Input Parameters**

The following input parameters were used:

#### **Gas Analysis**

| <b>Element</b>   | <b>Concentration</b> |
|------------------|----------------------|
| N <sub>2</sub>   | 0,0184               |
| CO <sub>2</sub>  | 0,0000               |
| H <sub>2</sub> S | 0,0260               |
| C <sub>1</sub>   | 0,7068               |
| C <sub>2</sub>   | 0,1414               |
| C <sub>3</sub>   | 0,0674               |
| iC <sub>4</sub>  | 0,0081               |
| nC <sub>4</sub>  | 0,0190               |
| iC <sub>5</sub>  | 0,0038               |
| nC <sub>5</sub>  | 0,0043               |
| C <sub>6</sub>   | 0,0026               |
| C <sub>7</sub>   | 0,0022               |

Ideal Gas relative density = 0,7792

### Meter Data (Downstream Flange Taps)

Meter Run I.D. = 52,3700mm

Orifice I.D. = 9,5250mm

### Flow Data (24Hrs)

Static Pressure = 2716.765 kPag

Differential Pressure = 10.2000 kPa

Flowing Temperature = 57.0000 oC

### Test Result

The results calculated by the module are listed below:

|                | Calculated Result | Theoretical Result | Actual Difference (percentage) | Actual Difference (percentage) | Result |
|----------------|-------------------|--------------------|--------------------------------|--------------------------------|--------|
| Cd             | 0.5990            | 0.5990             | 0.0000                         | 0.1000                         | PASS   |
| Y <sub>1</sub> | 0.9989            | 0.9989             | 0.0000                         | 0.0100                         | PASS*  |
| Ev             | 1.0006            | 1.0005             | 0.0100                         | 0.0100                         | PASS   |
| Zb             | 0.9959            | 0.9959             | 0.0000                         | 0.1000                         | PASS   |
| Zf             | 0.9277            | 0.9277             | 0.0000                         | 0.2000                         | PASS   |
| Q              | 2.7532            | 2.7532             | 0.0000                         | 0.2500                         | PASS   |

Where:

Cd = Orifice coefficient

Y<sub>1</sub> = Expansion Factor

Ev = Velocity of Approach

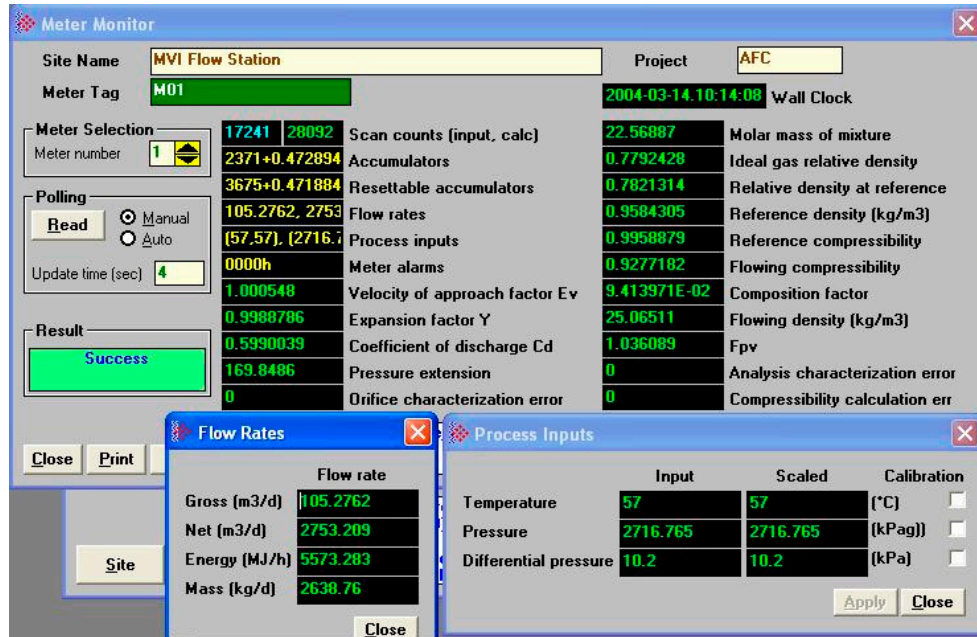
Zb = Reference Compressibility

Zf = Flowing Compressibility

Q = Flow Rate (103m<sup>3</sup>/24hours)

\* Since the result is rounded to four decimal places, a maximum tolerance of 0.01% is interpreted as the maximum absolute deviation of 0.0001. Since the Y<sub>1</sub> result is usually a value less than 1.0000, the result is considered valid if the difference between the calculated and the theoretical values is less or equal than 0.0001.

Follows below a screen shot of the AFC Manager Meter Monitor window which shows the data results for this test:



## 2.2 Test Case Number 2

### Input Parameters

The following input parameters were used:

### Gas Analysis

| Element          | Concentration |
|------------------|---------------|
| N <sub>2</sub>   | 0,0156        |
| CO <sub>2</sub>  | 0,0216        |
| H <sub>2</sub> S | 0,1166        |
| C <sub>1</sub>   | 0,7334        |
| C <sub>2</sub>   | 0,0697        |
| C <sub>3</sub>   | 0,0228        |
| iC <sub>4</sub>  | 0,0044        |
| nC <sub>4</sub>  | 0,0075        |
| iC <sub>5</sub>  | 0,0028        |
| nC <sub>5</sub>  | 0,0024        |
| C <sub>6</sub>   | 0,0017        |
| C <sub>7</sub>   | 0,0015        |

Ideal Gas relative density = 0,7456

**Meter Data (Downstream Flange Taps)**

Meter Run I.D. = 102,26mm

Orifice I.D. = 47,625mm

**Flow Data (24Hrs)**

Static Pressure = 8999,615 kPag

Differential Pressure = 11,0000 kPa

Flowing Temperature = 50.0000 oC

**Test Result**

The result calculated by the module:

|                | <b>Calculated Result</b> | <b>Theoretical Result</b> | <b>Actual Difference (percentage)</b> | <b>Actual Difference (percentage)</b> | <b>Result</b> |
|----------------|--------------------------|---------------------------|---------------------------------------|---------------------------------------|---------------|
| Cd             | 0.6019                   | 0.6019                    | 0.0000                                | 0.1000                                | PASS          |
| Y <sub>1</sub> | 0.9996                   | 0.9996                    | 0.0000                                | 0.0100                                | PASS*         |
| Ev             | 1.0244                   | 1.0244                    | 0.0000                                | 0.0100                                | PASS          |
| Zb             | 0.9967                   | 0.9967                    | 0.0000                                | 0.1000                                | PASS          |
| Zf             | 0.8097                   | 0.8097                    | 0.0000                                | 0.2000                                | PASS          |
| Q              | 146.1876                 | 146.1800                  | 0.0052                                | 0.2500                                | PASS          |

Where:

Cd = Orifice coefficient

Y<sub>1</sub> = Expansion Factor

Ev = Velocity of Approach

Zb = Reference Compressibility

Zf = Flowing Compressibility

Q = Flow Rate (103m<sup>3</sup>/24hours)

\* Since the result is rounded to four decimal places, a maximum tolerance of 0.01% is interpreted as the maximum absolute deviation of 0.0001. Since the Y<sub>1</sub> result is usually a value less than 1.0000, the result is considered valid if the difference between the calculated and the theoretical values is less or equal than 0.0001.

Follows below a screen shot of the AFC Manager Meter Monitor window which shows the data results for this test:



### 2.3 Test Case Number 3

#### Input Parameters

The following input parameters were used:

#### Gas Analysis

| Element          | Concentration |
|------------------|---------------|
| N <sub>2</sub>   | 0,0500        |
| CO <sub>2</sub>  | 0,1000        |
| H <sub>2</sub> S | 0,2000        |
| C <sub>1</sub>   | 0,6000        |
| C <sub>2</sub>   | 0,0500        |
| C <sub>3</sub>   | 0,0000        |
| iC <sub>4</sub>  | 0,0000        |
| nC <sub>4</sub>  | 0,0000        |
| iC <sub>5</sub>  | 0,0000        |
| nC <sub>5</sub>  | 0,0000        |
| C <sub>6</sub>   | 0,0000        |

| Element        | Concentration |
|----------------|---------------|
| C <sub>7</sub> | 0,0000        |

Ideal Gas relative density = 0,8199

### Meter Data (Downstream Flange Taps)

Meter Run I.D. = 590,55mm

Orifice I.D. = 304,80mm

### Flow Data (24Hrs)

Static Pressure = 10240,815 kPag

Differential Pressure = 22,1600 kPa

Flowing Temperature = 60.0000 oC

### Test Result

The result calculated by the module:

|                | Calculated Result | Theoretical Result | Actual Difference (percentage) | Actual Difference (percentage) | Result |
|----------------|-------------------|--------------------|--------------------------------|--------------------------------|--------|
| Cd             | 0.6029            | 0.6029             | 0.0000                         | 0.1000                         | PASS   |
| Y <sub>1</sub> | 0.9993            | 0.9993             | 0.0000                         | 0.0100                         | PASS*  |
| Ev             | 1.0375            | 1.0375             | 0.0000                         | 0.0100                         | PASS   |
| Zb             | 0.9968            | 0.9968             | 0.0000                         | 0.1000                         | PASS   |
| Zf             | 0.8213            | 0.8213             | 0.0000                         | 0.2000                         | PASS   |
| Q              | 8575.6480         | 8575.6000          | 0.0006                         | 0.2500                         | PASS   |

Where:

Cd = Orifice coefficient

Y<sub>1</sub> = Expansion Factor

Ev = Velocity of Approach

Zb = Reference Compressibility

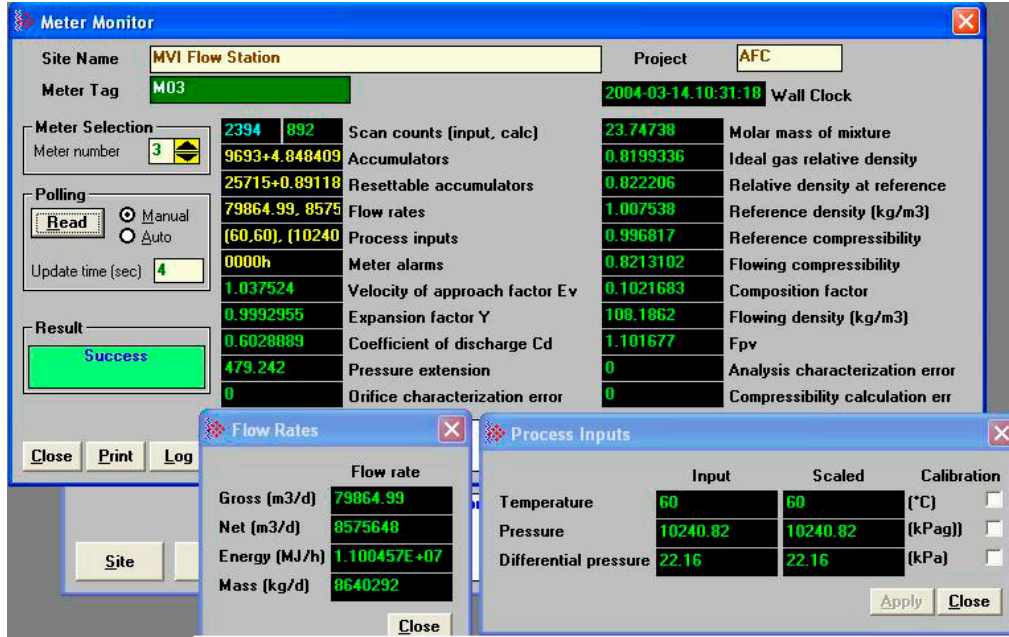
Zf = Flowing Compressibility

Q = Flow Rate (103m<sup>3</sup>/24hours)

\* Since the result is rounded to four decimal places, a maximum tolerance of 0.01% is interpreted as the maximum absolute deviation of 0.0001. Since the Y<sub>1</sub> result is usually a value less than 1.0000, the result is considered valid if the

difference between the calculated and the theoretical values is less or equal than 0.0001.

Follows below a screen shot of the AFC Manager Meter Monitor window which shows the data results for this test:



## 2.4 Test Case Number 4

### Input Parameters

The following input parameters were used:

### Gas Analysis

| Element          | Concentration |
|------------------|---------------|
| N <sub>2</sub>   | 0,0029        |
| CO <sub>2</sub>  | 0,0258        |
| H <sub>2</sub> S | 0,0000        |
| C <sub>1</sub>   | 0,9709        |
| C <sub>2</sub>   | 0,0003        |
| C <sub>3</sub>   | 0,0001        |
| iC <sub>4</sub>  | 0,0000        |
| nC <sub>4</sub>  | 0,0000        |
| iC <sub>5</sub>  | 0,0000        |
| nC <sub>5</sub>  | 0,0000        |

| Element        | Concentration |
|----------------|---------------|
| C <sub>6</sub> | 0,0000        |
| C <sub>7</sub> | 0,0000        |

Ideal Gas relative density = 0,5803

**Meter Data (Downstream Flange Taps)**

Meter Run I.D. = 146,36mm

Orifice I.D. = 88,9000mm

**Flow Data (24Hrs)**

Static Pressure = 9738,665 kPag

Differential Pressure = 6,6130 kPa

Flowing Temperature = 22,3500 oC

**Test Result**

The result calculated by the module:

|                | Calculated Result | Theoretical Result | Actual Difference (percentage) | Actual Difference (percentage) | Result |
|----------------|-------------------|--------------------|--------------------------------|--------------------------------|--------|
| Cd             | 0.6047            | 0.6047             | 0.0000                         | 0.1000                         | PASS   |
| Y <sub>1</sub> | 0.9998            | 0.9998             | 0.0000                         | 0.0100                         | PASS*  |
| Ev             | 1.0759            | 1.0759             | 0.0000                         | 0.0100                         | PASS   |
| Zb             | 0.9980            | 0.9980             | 0.0000                         | 0.1000                         | PASS   |
| Zf             | 0.8425            | 0.8425             | 0.0000                         | 0.2000                         | PASS   |
| Q              | 503.6474          | 503.6500           | 0.0005                         | 0.2500                         | PASS   |

Where:

Cd = Orifice coefficient

Y<sub>1</sub> = Expansion Factor

Ev = Velocity of Approach

Zb = Reference Compressibility

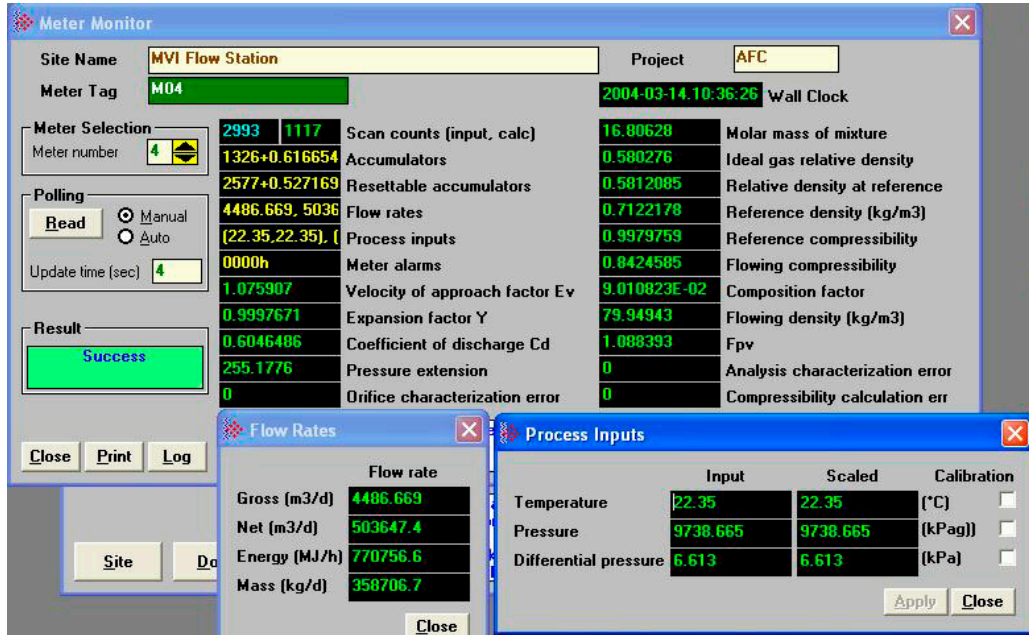
Zf = Flowing Compressibility

Q = Flow Rate (103m<sup>3</sup>/24hours)

\* Since the result is rounded to four decimal places, a maximum tolerance of 0.01% is interpreted as the maximum absolute deviation of 0.0001. Since the Y<sub>1</sub>

result is usually a value less than 1.0000, the result is considered valid if the difference between the calculated and the theoretical values is less or equal than 0.0001.

Follows below a screen shot of the AFC Manager Meter Monitor window which shows the data results for this test:



## 2.5 Test Case Number 5

### Input Parameters

The following input parameters were used:

### Gas Analysis

| Element          | Concentration |
|------------------|---------------|
| N <sub>2</sub>   | 0,0235        |
| CO <sub>2</sub>  | 0,0082        |
| H <sub>2</sub> S | 0,0021        |
| C <sub>1</sub>   | 0,7358        |
| C <sub>2</sub>   | 0,1296        |
| C <sub>3</sub>   | 0,0664        |
| iC <sub>4</sub>  | 0,0088        |
| nC <sub>4</sub>  | 0,0169        |
| iC <sub>5</sub>  | 0,0035        |

| Element         | Concentration |
|-----------------|---------------|
| nC <sub>5</sub> | 0,0031        |
| C <sub>6</sub>  | 0,0014        |
| C <sub>7</sub>  | 0,0007        |

Ideal Gas relative density = 0,7555

### Meter Data (Downstream Flange Taps)

Meter Run I.D. = 154,05mm

Orifice I.D. = 95,250mm

### Flow Data (24Hrs)

Static Pressure = 2398,575 kPag

Differential Pressure = 75,000 kPa

Flowing Temperature = 34,0 oC

### Test Result

The result calculated by the module:

|                | Calculated Result | Theoretical Result | Actual Difference (percentage) | Actual Difference (percentage) | Result |
|----------------|-------------------|--------------------|--------------------------------|--------------------------------|--------|
| Cd             | 0.6041            | 0.6042             | 0.0166                         | 0.1000                         | PASS   |
| Y <sub>1</sub> | 0.9898            | 0.9897             | 0.0101                         | 0.0100                         | PASS*  |
| Ev             | 1.0822            | 1.0822             | 0.0000                         | 0.0100                         | PASS   |
| Zb             | 0.9962            | 0.9962             | 0.0000                         | 0.1000                         | PASS   |
| Zf             | 0.9217            | 0.9217             | 0.0000                         | 0.2000                         | PASS   |
| Q              | 813.1285          | 813.0000           | 0.0158                         | 0.2500                         | PASS   |

Where:

Cd = Orifice coefficient

Y<sub>1</sub> = Expansion Factor

Ev = Velocity of Approach

Zb = Reference Compressibility

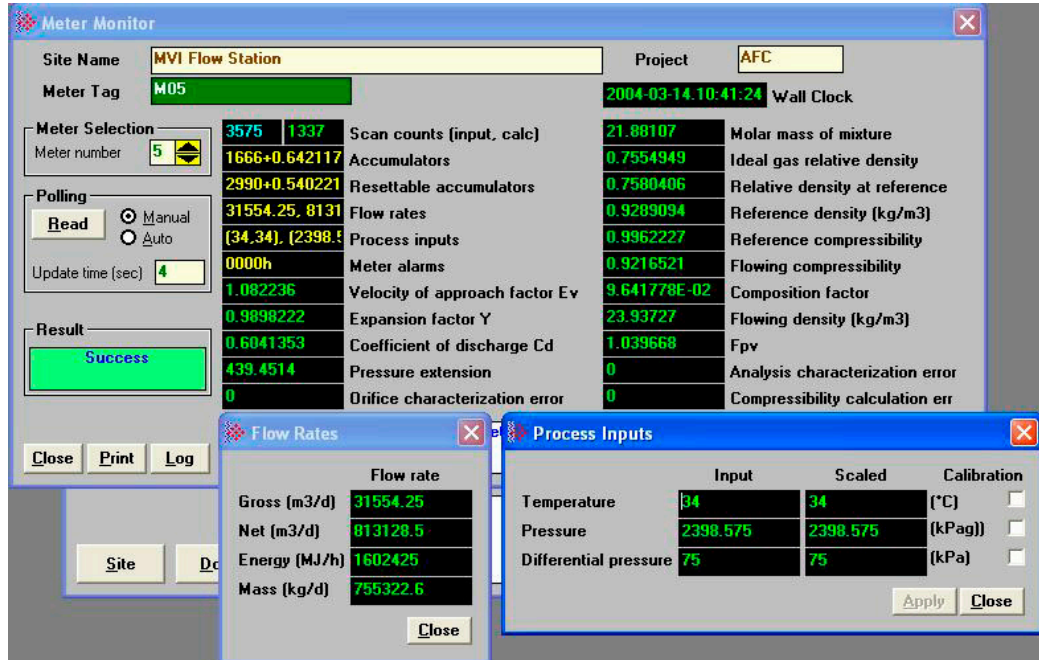
Zf = Flowing Compressibility

Q = Flow Rate (103m<sup>3</sup>/24hours)

\* Since the result is rounded to four decimal places, a maximum tolerance of 0.01% is interpreted as the maximum absolute deviation of 0.0001. Since the Y<sub>1</sub>

result is usually a value less than 1.0000, the result is considered valid if the difference between the calculated and the theoretical values is less or equal than 0.0001.

Follows below a screen shot of the AFC Manager Meter Monitor window which shows the data results for this test:



## 2.6 Test Case Number 6

### Input Parameters

The following input parameters were used:

### Gas Analysis

| Element          | Concentration |
|------------------|---------------|
| N <sub>2</sub>   | 0,0268        |
| CO <sub>2</sub>  | 0,0030        |
| H <sub>2</sub> S | 0,0000        |
| C <sub>1</sub>   | 0,6668        |
| C <sub>2</sub>   | 0,1434        |
| C <sub>3</sub>   | 0,1023        |
| iC <sub>4</sub>  | 0,0123        |
| nC <sub>4</sub>  | 0,0274        |

| Element         | Concentration |
|-----------------|---------------|
| iC <sub>5</sub> | 0,0000        |
| nC <sub>5</sub> | 0,0000        |
| C <sub>6</sub>  | 0,0180        |
| C <sub>7</sub>  | 0,0000        |

Ideal Gas relative density = 0,8377

**Meter Data (Downstream Flange Taps)**

Meter Run I.D. = 52,500mm

Orifice I.D. = 19,050mm

**Flow Data (24Hrs)**

Static Pressure = 2405,005 kPag

Differential Pressure = 17,0500 kPa

Flowing Temperature = 7,200 oC

**Test Result**

The result calculated by the module:

|                | Calculated Result | Theoretical Result | Actual Difference (percentage) | Actual Difference (percentage) | Result |
|----------------|-------------------|--------------------|--------------------------------|--------------------------------|--------|
| Cd             | 0.6005            | 0.6005             | 0.0000                         | 0.1000                         | PASS   |
| Y <sub>1</sub> | 0.9979            | 0.9978             | 0.0100                         | 0.0100                         | PASS*  |
| Ev             | 1.0088            | 1.0088             | 0.0000                         | 0.0100                         | PASS   |
| Zb             | 0.9951            | 0.9951             | 0.0000                         | 0.1000                         | PASS   |
| Zf             | 0.8578            | 0.8578             | 0.0000                         | 0.2000                         | PASS   |
| Q              | 14.7468           | 14.7460            | 0.0054                         | 0.2500                         | PASS   |

Where:

Cd = Orifice coefficient

Y<sub>1</sub> = Expansion Factor

Ev = Velocity of Approach

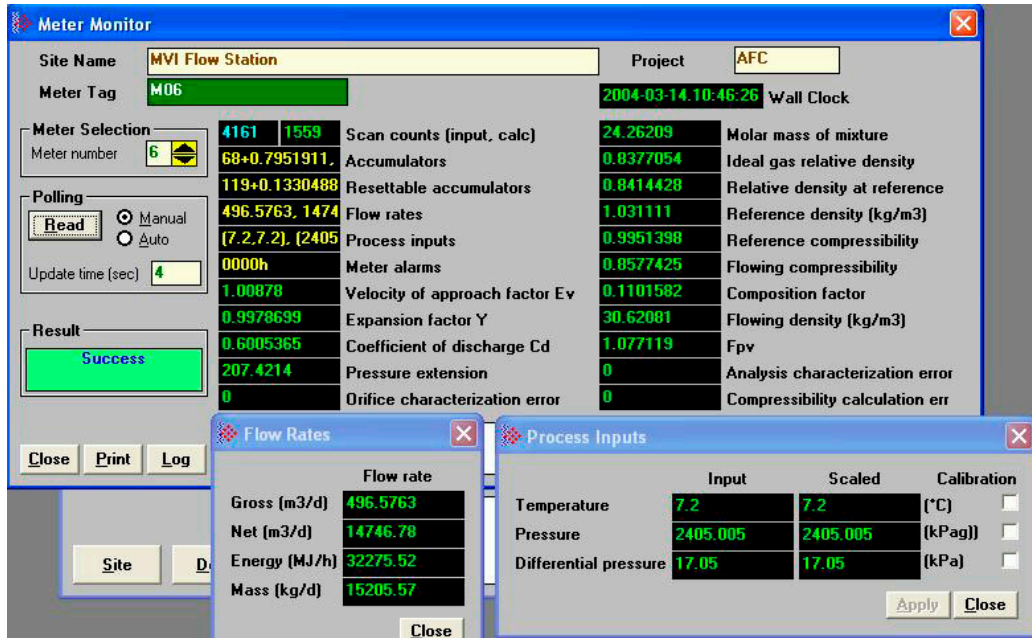
Zb = Reference Compressibility

Zf = Flowing Compressibility

Q = Flow Rate (103m<sup>3</sup>/24hours)

\* Since the result is rounded to four decimal places, a maximum tolerance of 0.01% is interpreted as the maximum absolute deviation of 0.0001. Since the Y1 result is usually a value less than 1.0000, the result is considered valid if the difference between the calculated and the theoretical values is less or equal than 0.0001.

Follows below a screen shot of the AFC Manager Meter Monitor window which shows the data results for this test:

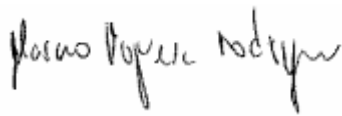




### 3 Conclusion

The tests demonstrated that the MVI71-AFC correctly calculates the AGA results listed in this document considering the accuracy according to Guide 46 document from the Alberta Energy and Utilities Board (EUB).

These tests were conducted by Eng Marcio N Rodrigues and were concluded on March 15th, 2004.



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